

# Incompressible Stokes flow in an annulus: An analytical solution and numerical benchmark

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## Abstract

We present a new family of analytical solutions to the incompressible Stokes equation in an annulus with a constant viscosity, a gravity field that points towards the center of the annulus, and a density field that depends on the spatial coordinates. The velocity is tangential to both the inner and the outer boundaries and is such that it produces convection cells, the number of which is parametrized by a single parameter  $k$ . This benchmark has been implemented in the finite element geodynamics codes ASPECT and ELEFANT. We report convergence rates for the velocity and pressure as well as global velocity averages.

*Keywords:* Finite Element Method; Incompressible Stokes equations; Incompressible Stokes flow in an annulus; Benchmark for Stokes flow in an annulus;

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<sup>1</sup> Authors CT and EGP derived the analytical benchmark together. CT implemented the benchmark in both ASPECT and ELEFANT codes. CT and EGP wrote the manuscript together.

## 10 **1. Introduction**

Numerical modeling is an essential component of our understanding of convection in the Earth's  
mantle [1] as it allows geodynamicists to test hypotheses and build ever more refined models of  
mantle processes. Given the vastly different time scales of the dynamics of the core from that of  
the mantle and the vast differences between the rheologies of these two regions, rather than using  
computer models in spheres researchers have developed two dimensional models of the Earth's mantle  
in annuli [2, 3, 4, 5, 6, 7, 8, 9] and three dimensional models in spherical shells [10, 11, 12, 13, 14,  
15, 16].

While there are only a few analytical and numerical benchmarks in 3D spherical shells [12, 14, 17]  
there are a great many on rectangular grids in rectangular, two-dimensional Cartesian domains [18, 19,  
20, 21, 22]. However, to our knowledge, there are no non-trivial, incompressible, isoviscous, and  
isothermal benchmarks that involve an exact solution of the incompressible Stokes equations in a  
two-dimensional annulus.

We have developed such a benchmark for an isoviscous, isothermal solution of the incompressible  
Stokes equations for which simple kinematic boundary conditions lead to structures that serve  
as a model of “convection cells”, where the number of these cells is determined by a single param-  
eter  $k$ . These cells are kinematic, isothermal counterparts of those found in full mantle convection  
experiments and computations.

In Section 2 we present the derivation of our analytical solution to the isoviscous, isothermal in-  
compressible Stokes equations in an annulus and in Section 3 we compare our numerical computations  
of these solutions with the exact analytical solution.

## **2. Derivation of the Exact Solution**

We seek an exact solution to the incompressible Stokes equations for an isoviscous, isothermal  
fluid in an annulus. Given the geometry of the problem, we work in polar coordinates. We denote  
the orthonormal basis vectors by  $\mathbf{e}_r$  and  $\mathbf{e}_\theta$ , the inner radius of the annulus by  $R_1$  and the outer  
radius by  $R_2$ . Further, we assume that the viscosity  $\mu$  is constant, which we set to  $\mu = 1$  we set the  
gravity vector to  $\mathbf{g} = -g_r \mathbf{e}_r$  with  $g_r = 1$ .

Given these assumptions, the incompressible Stokes equations in the annulus are [23]

$$\frac{\partial^2 v_r}{\partial r^2} + \frac{1}{r} \frac{\partial v_r}{\partial r} + \frac{1}{r^2} \frac{\partial^2 v_r}{\partial \theta^2} - \frac{v_r}{r^2} - \frac{2}{r^2} \frac{\partial u_\theta}{\partial \theta} - \frac{\partial p}{\partial r} - \rho g_r = 0 \quad (1)$$

$$\frac{\partial^2 v_\theta}{\partial r^2} + \frac{1}{r} \frac{\partial v_\theta}{\partial r} + \frac{1}{r^2} \frac{\partial^2 v_\theta}{\partial \theta^2} + \frac{2}{r^2} \frac{\partial v_r}{\partial \theta} - \frac{v_\theta}{r^2} - \frac{1}{r} \frac{\partial p}{\partial \theta} = 0 \quad (2)$$

$$\frac{1}{r} \frac{\partial(r v_r)}{\partial r} + \frac{1}{r} \frac{\partial v_\theta}{\partial \theta} = 0 \quad (3)$$

38 Equations (1) and (2) are the momentum equations in polar coordinates while Equation (3) is the  
incompressibility constraint.

40 We now postulate the  $\theta$ -component of velocity vector can be written as

$$v_\theta(r, \theta) = f(r) \cos(k\theta) \quad (4)$$

where the function  $f(r)$  will be specified later. From Equation (3) we can write

$$\frac{\partial(rv_r)}{\partial r} = -\frac{\partial v_\theta}{\partial \theta} = kf(r) \sin(k\theta) \quad (5)$$

42 leading to

$$v_r(r, \theta) = g(r)k \sin(k\theta) \quad (6)$$

where

$$g(r) = \frac{1}{r} \int f(r) dr \quad (7)$$

44 Since the velocity is tangential to both boundaries we have

$$v_r(r = R_1, \theta) = v_r(r = R_2, \theta) = 0 \quad (8)$$

for all  $\theta \in [0, 2\pi]$ . By taking  $f(r) = Ar + B/r$ , (e.g., see the solution of the Laplace equation in an  
46 annulus in [24] for  $n = 0, 1$ ) one obtains

$$g(r) = \frac{A}{2}r + \frac{B}{r} \ln r + \frac{C}{r} \quad (9)$$

where  $C$  is a non-zero constant of integration. Given the boundary conditions in Equation (8) we  
48 find that

$$A = -C \frac{2(\ln R_1 - \ln R_2)}{R_2^2 \ln R_1 - R_1^2 \ln R_2} \quad (10)$$

$$B = -C \frac{R_2^2 - R_1^2}{R_2^2 \ln R_1 - R_1^2 \ln R_2} \quad (11)$$

Thus,

$$\frac{\partial^2 f}{\partial r^2} + \frac{1}{r} \frac{\partial f}{\partial r} - \frac{f}{r^2} = 0 \quad (12)$$

50 so that Equation (2) simplifies to

$$\frac{1}{r^2} \frac{\partial^2 v_\theta}{\partial \theta^2} + \frac{2}{r^2} \frac{\partial v_r}{\partial \theta} - \frac{1}{r} \frac{\partial p}{\partial \theta} = 0 \quad (13)$$

which leads to

$$p(r, \theta) = kh(r) \sin(k\theta) + l(r) \quad (14)$$

52 where  $l(r)$  comes from integration with respect to  $\theta$  and  $h(r) = (2g(r) - f(r))/r$ . We now insert  
Equation (14) into Equation (1) to obtain

$$\begin{aligned}
\rho(r, \theta) &= \frac{\partial^2 v_r}{\partial r^2} + \frac{1}{r} \frac{\partial v_r}{\partial r} + \frac{1}{r^2} \frac{\partial^2 v_r}{\partial \theta^2} - \frac{v_r}{r^2} - \frac{2}{r^2} \frac{\partial v_\theta}{\partial \theta} - \frac{\partial p}{\partial r} \\
&= kg''(r) \sin(k\theta) + k \frac{g'(r)}{r} \sin(k\theta) - k^3 \frac{g(r)}{r^2} \sin(k\theta) \\
&\quad - k \frac{g(r)}{r^2} \sin(k\theta) + k \frac{2f(r)}{r^2} \sin(k\theta) - kh'(r) \sin(k\theta) - l'(r) \\
&= \mathcal{M}(r)k \sin(k\theta) - l'(r)
\end{aligned} \tag{15}$$

54 where

$$\mathcal{M}(r) = g'' - \frac{g'}{r} - \frac{g}{r^2}(k^2 - 1) + \frac{f}{r^2} + \frac{f'}{r}. \tag{16}$$

Taking  $k = 0$  yields  $\rho(r, \theta) = -l'(r)$ , so we choose  $l'(r) = -\rho_0$ . In this case,

$$p(r, \theta)|_{k=0} = l(r) = \rho_0 g_r (R_2 - r) \tag{17}$$

56 where we have imposed  $p(r, \theta) = 0$  at the outer radius  $r = R_2$ .

Equations (4), (6), and (14) are a solution of the incompressible Stokes equations. In Figure 1  
58 we present the velocity and pressure fields for  $k = 0, 1, 2$ , and 4 and  $\rho_0 = 0$ . For  $k = 0$  the velocity  
is tangential to both the inner and outer boundaries: it is clockwise on the inner boundary  $r = R_1$   
60 and counterclockwise on the outer boundary,  $r = R_2$ . thereby imposing a shear flow in the annulus.  
The density is purely radial as is the pressure. When  $k > 0$  there are  $k$  cells or ‘lobes’ with positive  
62 density values and  $k$  lobes with negative values, yielding  $2k$  convection cells.

### 2.1. Average Benchmark Quantities

64 Benchmark publications often focus on scalar quantities that represent the solution in an average  
sense [18, 25]. Often these quantities are velocity averages or root mean square velocities. Since we  
66 have an exact expression for the velocity field, we can compute the exact analytical value of these  
averages.

- 68 •  $\theta$ -average of radial velocity component  $v_r$ ,

$$\langle v_r(r) \rangle = \frac{1}{2\pi} \int_0^{2\pi} v_r(r, \theta) d\theta = 0 \tag{18}$$

- $\theta$ -average of the velocity component  $v_\theta$ ,

$$\langle v_\theta(r) \rangle = \frac{1}{2\pi} \int_0^{2\pi} v_\theta(r, \theta) d\theta = 0 \tag{19}$$

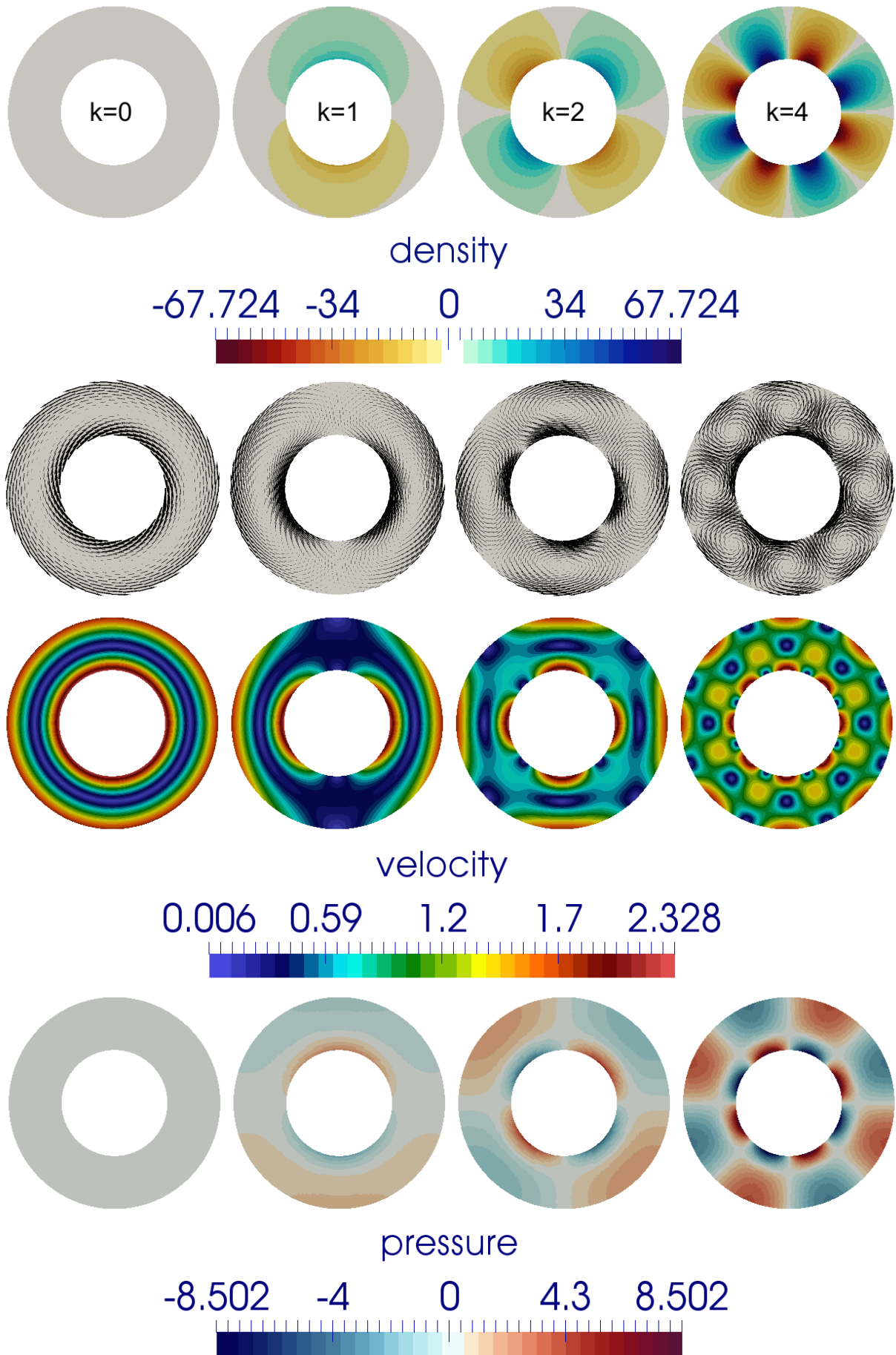


Figure 1: From left to right, increasing values of  $k$ . From top to bottom, density given by Equation (15), velocity vectors and magnitude given by Equations (4) and (6), and pressure given by Equation (14).

- 70 •  $\theta$ -root mean square average of the velocity component  $v_r$

$$\langle v_r(r) \rangle_{rms} = \sqrt{\frac{1}{2\pi} \int_0^{2\pi} v_r(r, \theta)^2 d\theta} = \frac{k|g(r)|}{\sqrt{2}} \quad (20)$$

- $\theta$ -root mean square average of the velocity component  $v_\theta$

$$\langle v_\theta \rangle_{rms}(r) = \sqrt{\frac{1}{2\pi} \int_0^{2\pi} v_\theta(r, \theta)^2 d\theta} = \frac{|f(r)|}{\sqrt{2}} \quad (21)$$

- 72 • Root mean square velocity  $v_{rms}$

$$v_{rms} = \sqrt{\frac{1}{V} \int_V (v_r^2 + v_\theta^2) dV} \quad (22)$$

where  $V$  is the volume (area) of the annulus. When  $k = 0$ , the root mean square velocity is given by:

74

$$\begin{aligned} v_{rms} &= \sqrt{\frac{1}{V} \int_0^{2\pi} d\theta \int_{R_1}^{R_2} f(r)^2 r dr} \\ &= \sqrt{\frac{2}{(R_2^2 - R_1^2)} \left[ \frac{A^2}{4} (R_2^4 - R_1^4) + AB(R_2^2 - R_1^2) + B^2(\ln R_2 - \ln R_1) \right]} \end{aligned} \quad (23)$$

When  $k = 1$ , the root mean square velocity is given by:

$$\begin{aligned} v_{rms} &= \sqrt{\frac{1}{V} \int_0^{2\pi} \int_{R_1}^{R_2} [(f(r) \cos(k\theta))^2 + (g(r)k \sin(k\theta))^2] r dr d\theta} \\ &= \left( \frac{A^2}{16} (4 + k^2) (R_2^4 - R_1^4) + \left( \frac{AB}{4} (4 - k^2) + \frac{ACk^2}{2} \right) (R_2^2 - R_1^2) \right. \\ &\quad + (B^2 + C^2 k^2) (\ln R_2 - \ln R_1) + BCk^2 [(\ln R_2)^2 - (\ln R_1)^2] \\ &\quad \left. + \frac{B^2 k^2}{3} [(\ln R_2)^3 - (\ln R_1)^3] + \frac{ABk^2}{2} [R_2^2 \ln R_2 - R_1^2 \ln R_1] \right)^{1/2} \\ &\quad / (R_2^2 - R_1^2)^{1/2} \end{aligned} \quad (24)$$

### 76 3. Numerical Results

The solution to the incompressible Stokes equations that we derived in Section 2 above is intended to be a numerical benchmark. In this case, the velocity is only prescribed on the inner and outer boundaries  $r = R_1, R_2$  and in what follows we have set  $\rho_0 = 0$ .

78

80 The density is then given by Equation (15), the gravity vector is  $\mathbf{g} = -\mathbf{e}_r$ , and we set  $C = -1$ ,  
81  $R_1 = 1$ , and  $R_2 = 2$ .

82 We used two different computer codes to compute the following results.

- 83 • ELEFANT<sup>2</sup> is a FEM code [17, 26, 27] that is a successor to the FANTOM code [28], but which  
84 also has a number of improvements as compared to its predecessor. It is a finite element code  
85 that supports both triangular and quadrilateral elements. In this work we used the  $Q_1 \times P_0$   
86 element combination.
- 87 • ASPECT<sup>3</sup> (Advanced Solver for Problems in Earths ConvecTion) is an open source finite  
88 element code [29, 30, 31]. It is built upon deal.II [32], which is a general-purpose FEM library,  
89 TRILINOS [33], which provides scalable and parallel solvers, and p4est [34], which builds  
90 distributed, parallelized, adaptive meshes. ASPECT relies on the use of modern numerical  
91 methods, such as adaptive mesh refinement, linear and nonlinear solvers, and stabilization of  
92 transport-dominated processes. These modern methods, together with high-order elements,  
93 ensure highly accurate solutions and excellent parallel scaling that has been demonstrated for  
94 up to several thousand processors. For the benchmark problems presented in this paper we  
95 used the  $Q_2 \times Q_1$  element combination in ASPECT on uniform grids. The present benchmark  
96 is implemented in ASPECT 2.0 and is referenced in the ASPECT users' manual [35].

97 In our computations, the finite element grids contain  $n_{el} = n_r * n_t$  elements where  $n_r$  is the number  
98 of elements in the radial direction and  $n_t$  is the number of elements in the  $\theta$  direction. One can check  
99 the correctness of our implementation by examining the computed pressure on the two boundaries  
100 in Figure 2, which shows both the computed and true pressures for  $k = 1, 2$ , and 4. One can see  
101 that there is excellent agreement between the computed values and the analytical values. The error  
102 in the computed pressure field is further documented in Figure 5.

103 In Figures 3 we show the computed values of the average velocities for various values of  $k$ , where  
104 the true values are from Equations (18) and (19). Note that the difference between the computed and  
105 exact values are on the order of machine precision  $\mu = 10^{-16}$ . In Figure 4a,b we show the computed  
106 radial and tangential root mean square velocities as compared to the true values in Equations (20)  
107 and (21). The computed and analytical profiles are indistinguishable in this Figure. We computed  
108 the root mean square velocity for various values of  $k$  and various resolutions. The values we obtained  
with ASPECT and ELEFANT are reported in Table 1. It is apparent that the measured values

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<sup>2</sup><http://cedricthieulot.net/elefant.html>

<sup>3</sup><https://aspect.geodynamics.org/>

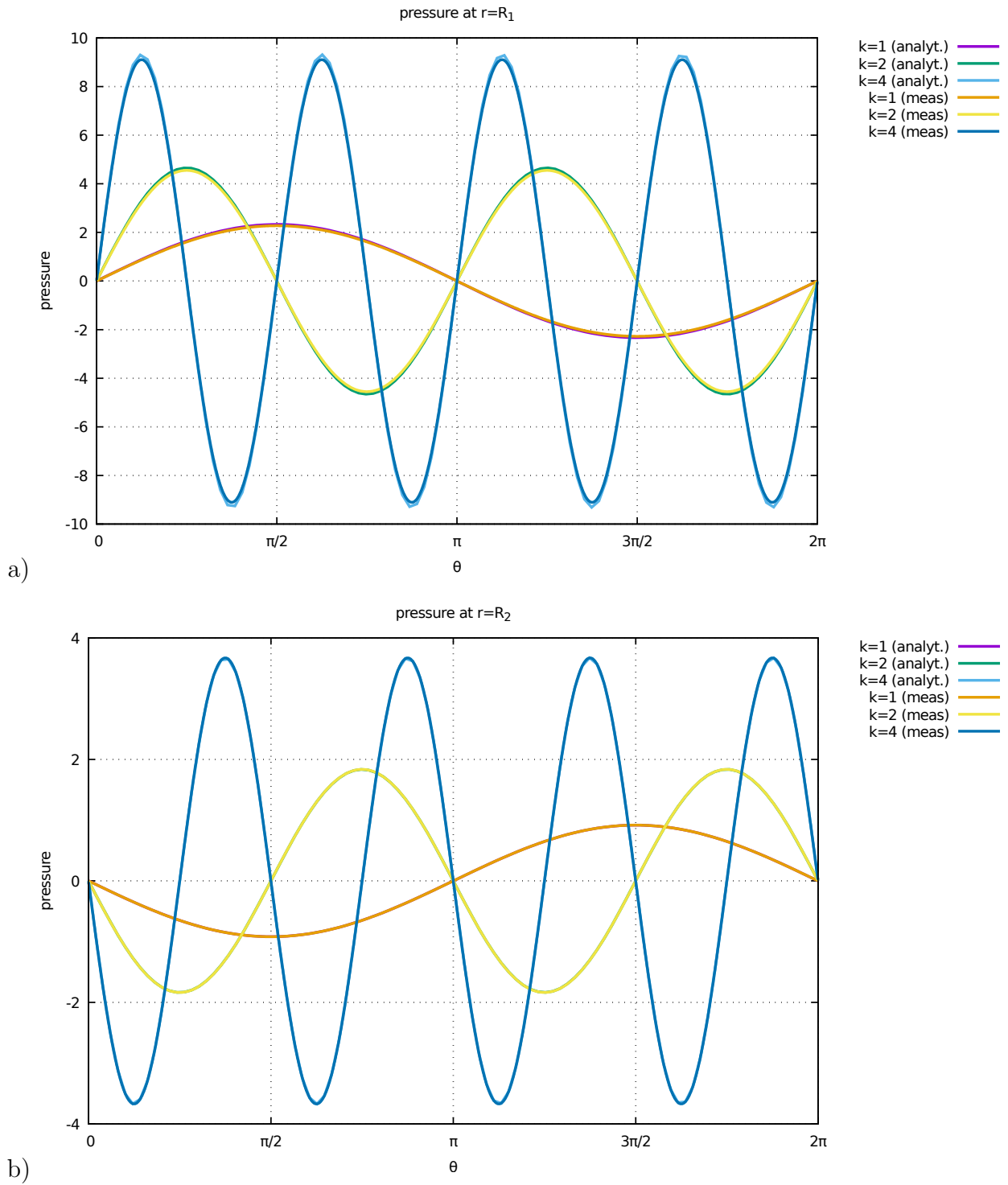
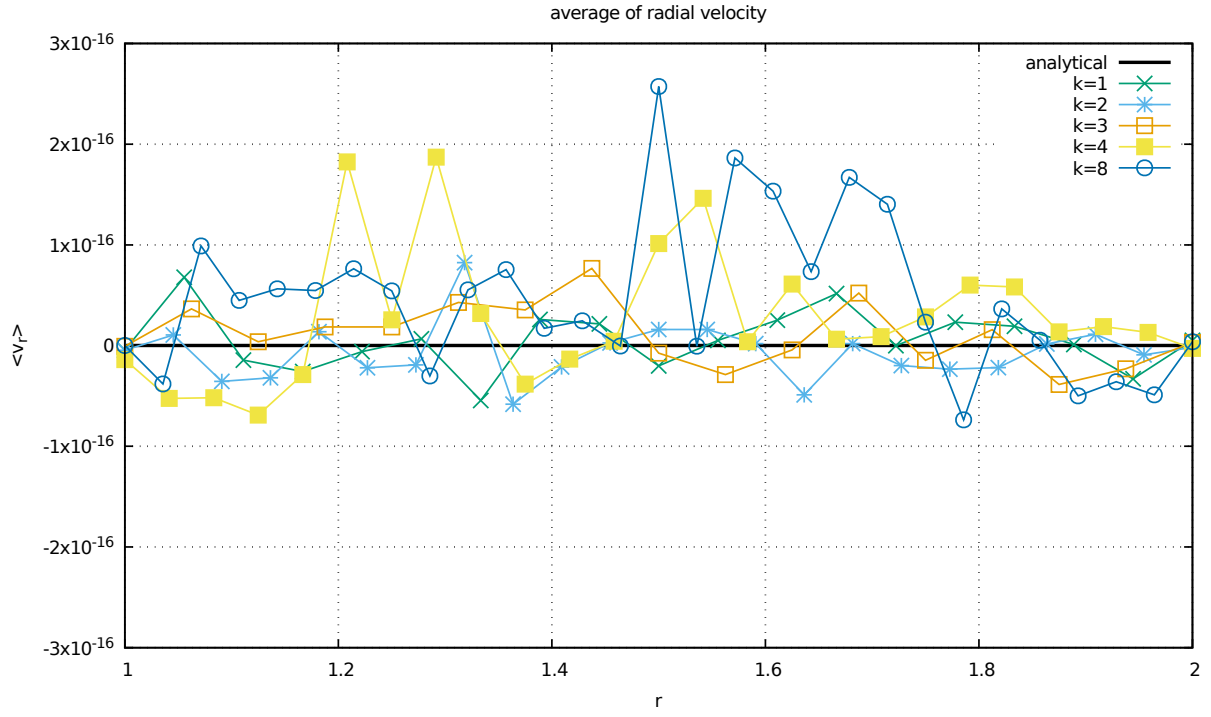
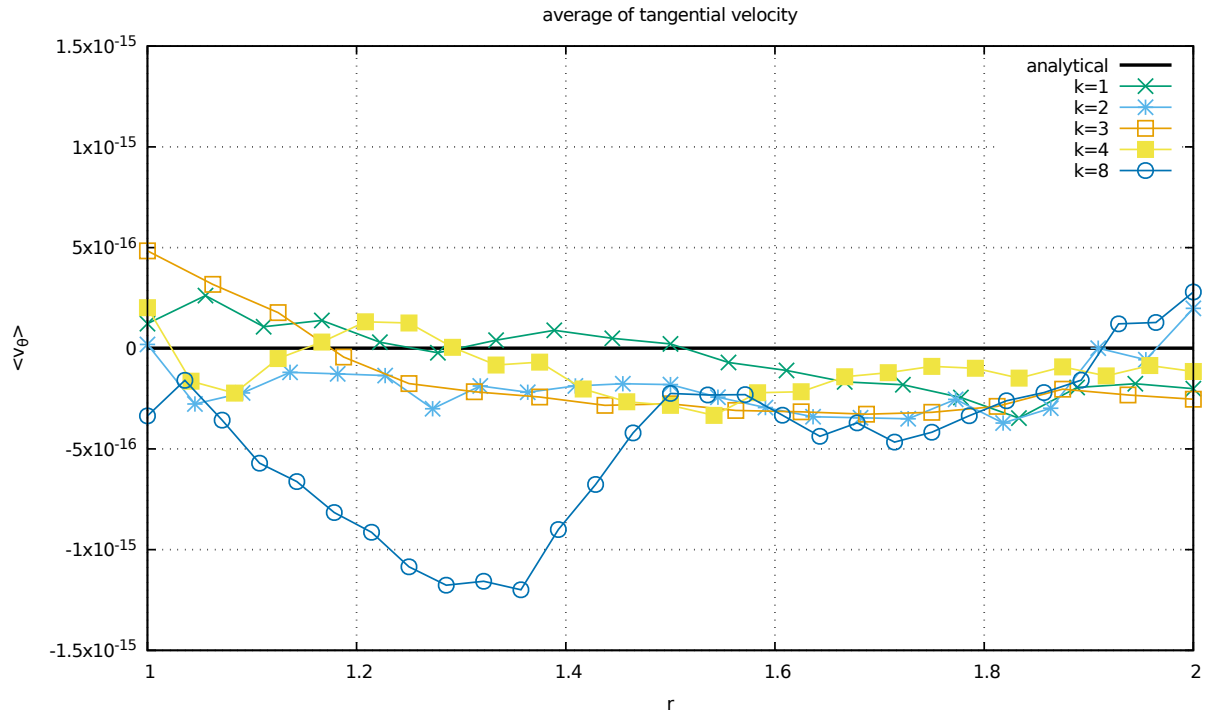


Figure 2: The pressure on a) the inner boundary  $r = R_1$ ; b) the outer boundary  $r = R_2$  obtained with ELEFANT. The grid resolution is  $n_r = 128$  elements in the radial direction and  $n_t = 1024$  elements in the tangential direction.





a)



b)

Figure 3: Computed radial averages of the (a) radial and (b) tangential velocity components as a function of  $r$  for  $k = 1, 2, 3, 4$ , and 8 versus the true values from Equations (18) and (19). Results obtained with ELEFANT.

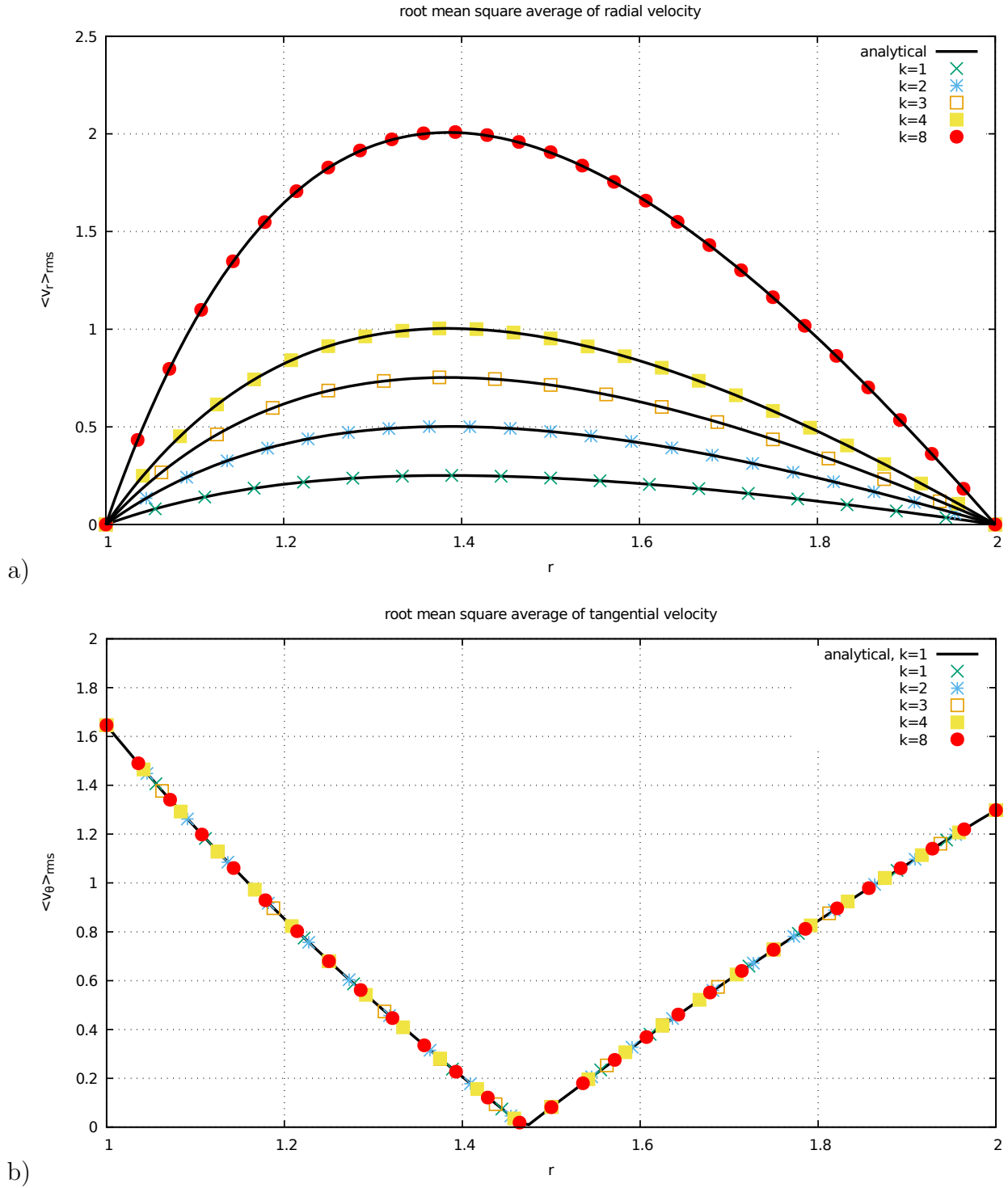


Figure 4: Root mean square (a) radial and (b) tangential velocity components as a function of  $r$  for  $k = 1, 2, 3, 4, 8$ . Results obtained with ELEFANT. .

$n_r * n_t$	k=0	k=1	k=2	k=3	k=4	k=8
ELEFANT						
8x128	1.16053	0.83943	0.89217	0.97388	1.07810	1.61846
16x256	1.15957	0.83883	0.89280	0.97618	1.08222	1.63256
32x512	1.15932	0.83868	0.89295	0.97674	1.08322	1.63609
64x1024	1.15926	0.83864	0.89299	0.97688	1.08347	1.63697
128x2048	1.15924	0.83863	0.89300	0.97692	1.08353	1.63719
256x4096	1.15924	0.83863	0.89300	0.97693	1.08355	1.63724
ASPECT						
$4 \times 48$	1.157773	0.8377398	0.89250634	0.9769904	1.0842358	1.638336
$8 \times 96$	1.158835	0.8383679	0.89280005	0.9768007	1.0835105	1.637383
$16 \times 192$	1.159134	0.8385620	0.89294820	0.9768854	1.0835267	1.637273
$32 \times 384$	1.159211	0.8386131	0.89299078	0.9769167	1.0835465	1.637261
$64 \times 768$	1.159230	0.8386260	0.8930018	0.9769253	1.0835525	1.637260
$128 \times 1536$	1.159235	0.8386293	0.8930046	0.9769275	1.0835540	1.637259
Analytical	1.159236712	0.8386303476	0.8930054915	0.9769282067	1.083554613	1.637259224

Table 1: Root mean square velocity values for various values of  $k$  and grid resolutions for both ELEFANT and ASPECT.

110 converge to the analytical one as the mesh size  $h = (R_2 - R_1)/n_r$  is decreased.

112 Finally, we investigate how the error in the computed solution diminishes with an increase of  
114 resolution. We then compute the  $L_2$ -norm of the error [36] for both velocity and pressure and plot  
116 these as a function of resolution and for various values of  $k$ . The resolution varied from  $8 \times 128$  to  
 $512 \times 8192$ . We see that the velocity error converges like  $\mathcal{O}(h^{n+1})$  while the pressure error converges  
like  $\mathcal{O}(h^n)$  for  $Q^n \times Q^{n-1}$  elements as shown in Figure 5. We also computed this test in ASPECT  
with  $Q_2 \times P_{-1}$  elements with nearly identical results. All error measurement values are available in  
[Appendix A](#).

## 118 4. Conclusions

We have derived a family of analytical solutions to the incompressible Stokes equations for an  
120 isoviscous, isothermal fluid in an annulus. These solutions were implemented in two geodynamic codes,  
ASPECT and ELEFANT, and the accuracy of the computed solutions was checked for three finite  
122 elements combinations:  $Q_1 \times P_0$ ,  $Q_2 \times Q_1$ , and  $Q_3 \times Q_2$ . The convergence rates were shown to be  
as expected from the theory of finite element methods for the incompressible Stokes equations. WE  
124 also derived several velocity field averages analytically and demonstrated that the computed values  
were in excellent agreement with the analytical values. Given the nature of the flow, which made  
126 up of multiple convection cells with tangential flow on the boundaries, we expect that this family of  
analytical solutions will become a standard benchmark for advection methods in annular geometries.

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134 2016.

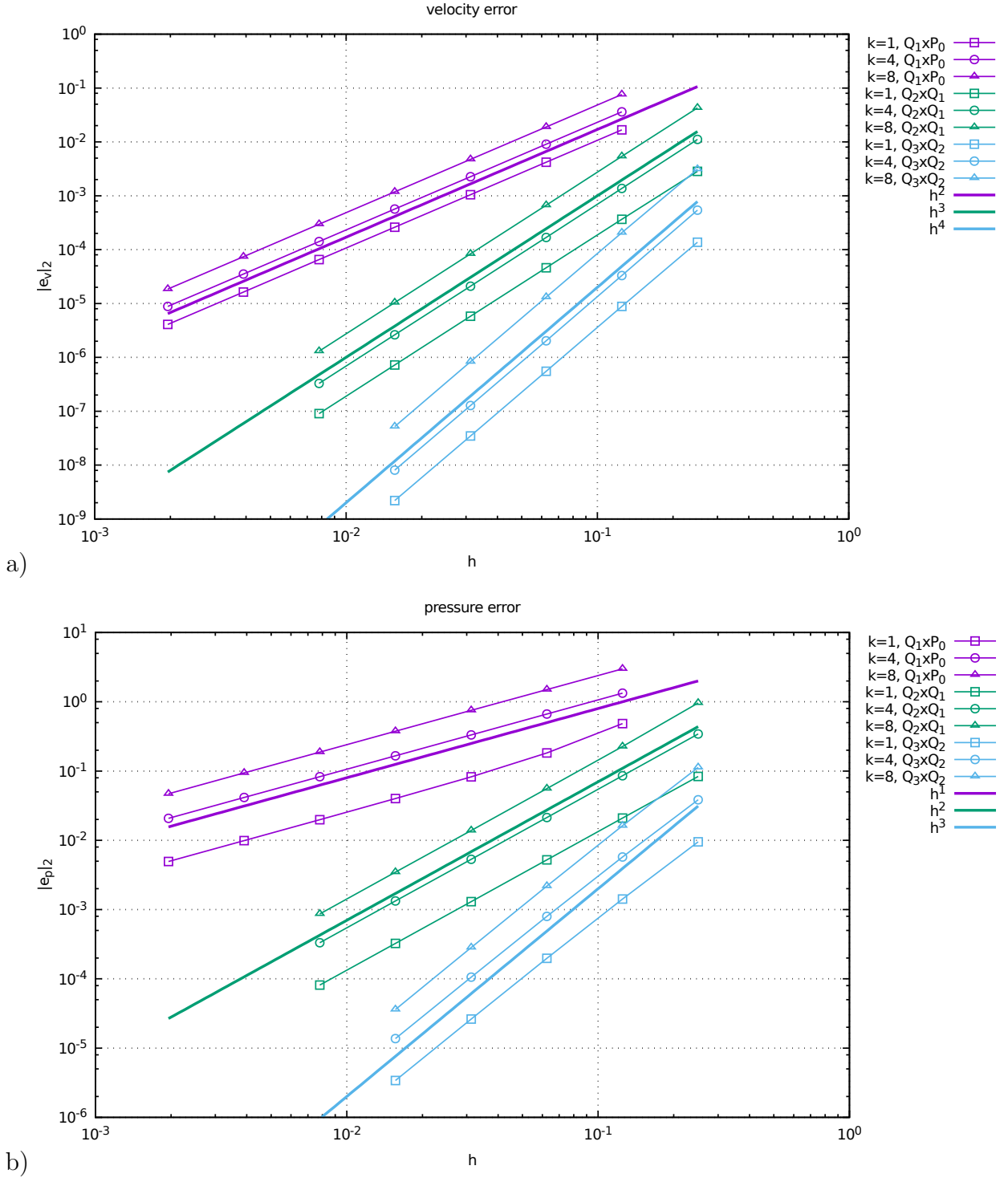


Figure 5: a)  $L_2$ -norm of the error in velocity as a function of the grid resolution  $h$ ; b)  $L_2$ -norm of the error in the pressure as a function of  $h$ . ( $Q_1 \times P_0$  results obtained with ELEFANT,  $Q_2 \times Q_1$  and  $Q_3 \times Q_2$  results obtained with ASPECT).

## Appendix A. TABLES OF ERRORS

In the following tables the velocity and pressure errors of Fig. (5) are reported as well as the corresponding convergence rates which are defined as:

$$\text{rate} = \log_2 \left( \frac{\text{err}(h = 2^{n-1})}{\text{err}(h = 2^n)} \right)$$

**ELEFANT** ( $Q_1 \times P_0$ ):

	$ e_v _2$	rate	$ e_p _2$	rate	$ e_v _2$	rate	$ e_p _2$	rate	$ e_v _2$	rate	$ e_p _2$	rate
	$(k=1)$			$(k=4)$			$(k=8)$			$(k=8)$		
8	$1.6726 \times 10^{-2}$	2.00	$4.8376 \times 10^{-1}$	1.41	$3.6136 \times 10^{-2}$	2.00	$1.3340 \times 10^{+0}$	2.00	$7.5685 \times 10^{-2}$	2.00	$2.9939 \times 10^{+0}$	2.00
16	$4.1829 \times 10^{-3}$	2.00	$1.8261 \times 10^{-1}$	1.41	$9.0391 \times 10^{-3}$	2.00	$6.6485 \times 10^{-1}$	2.00	$1.8932 \times 10^{-2}$	2.00	$1.5019 \times 10^{+0}$	2.00
32	$1.0458 \times 10^{-3}$	2.00	$8.2440 \times 10^{-2}$	1.15	$2.2600 \times 10^{-3}$	2.00	$3.3215 \times 10^{-1}$	2.00	$4.7328 \times 10^{-3}$	2.00	$7.5156 \times 10^{-1}$	2.00
64	$2.6146 \times 10^{-4}$	2.00	$4.0041 \times 10^{-2}$	1.04	$5.6503 \times 10^{-4}$	2.00	$1.6604 \times 10^{-1}$	2.00	$1.1831 \times 10^{-3}$	2.00	$3.7586 \times 10^{-1}$	2.00
128	$6.5366 \times 10^{-5}$	2.00	$1.9870 \times 10^{-2}$	1.01	$1.4126 \times 10^{-4}$	2.00	$8.3016 \times 10^{-2}$	2.00	$2.9579 \times 10^{-4}$	2.00	$1.8793 \times 10^{-1}$	2.00
256	$1.6341 \times 10^{-5}$	2.00	$9.9165 \times 10^{-3}$	1.00	$3.5315 \times 10^{-5}$	2.00	$4.1507 \times 10^{-2}$	2.00	$7.3949 \times 10^{-5}$	2.00	$9.3971 \times 10^{-2}$	2.00
512	$4.0854 \times 10^{-6}$	2.00	$4.9559 \times 10^{-3}$	1.00	$8.8287 \times 10^{-6}$	2.00	$2.0753 \times 10^{-2}$	2.00	$1.8487 \times 10^{-5}$	2.00	$4.6985 \times 10^{-2}$	2.00

**ASPECT** ( $Q_2 \times Q_1$ )

	$ e_v _2$	rate	$ e_p _2$	rate	$ e_v _2$	rate	$ e_p _2$	rate	$ e_v _2$	rate	$ e_p _2$	rate
	$(k=1)$			$(k=4)$			$(k=8)$			$(k=8)$		
4	$2.8334 \times 10^{-3}$	2.95	$8.3514 \times 10^{-2}$	2.00	$1.1138 \times 10^{-2}$	3.02	$3.4266 \times 10^{-1}$	3.00	$4.2895 \times 10^{-02}$	3.00	$9.6314 \times 10^{-1}$	2.09
8	$3.6567 \times 10^{-4}$	2.99	$2.0923 \times 10^{-2}$	2.00	$1.3661 \times 10^{-3}$	3.02	$8.5717 \times 10^{-2}$	3.01	$5.3779 \times 10^{-03}$	3.01	$2.2629 \times 10^{-1}$	2.02
16	$4.6179 \times 10^{-5}$	3.00	$5.2107 \times 10^{-3}$	2.00	$1.6856 \times 10^{-4}$	3.00	$2.1341 \times 10^{-2}$	3.00	$6.6867 \times 10^{-04}$	3.00	$5.5718 \times 10^{-2}$	2.01
32	$5.7907 \times 10^{-6}$	3.00	$1.3001 \times 10^{-3}$	2.00	$2.0998 \times 10^{-5}$	3.00	$5.3248 \times 10^{-3}$	3.00	$8.3418 \times 10^{-05}$	3.00	$1.3874 \times 10^{-2}$	2.00
64	$7.2452 \times 10^{-7}$	3.00	$3.2482 \times 10^{-4}$	2.00	$2.6230 \times 10^{-6}$	3.00	$1.3303 \times 10^{-3}$	3.00	$1.0422 \times 10^{-05}$	3.00	$3.4651 \times 10^{-3}$	2.00
128	$9.0590 \times 10^{-8}$	3.00	$8.1192 \times 10^{-5}$	2.00	$3.2786 \times 10^{-7}$	3.00	$3.3254 \times 10^{-4}$	3.00	$1.3028 \times 10^{-06}$	3.00	$8.6605 \times 10^{-4}$	2.00

ASPECT ( $Q_3 \times Q_2$ )

	$ e_v _2$	rate	$ e_p _2$	rate	$ e_v _2$	rate	$ e_p _2$	rate	$ e_v _2$	rate	$ e_p _2$	rate
	$(k=1)$			$(k=4)$			$(k=8)$			$(k=8)$		
4	$1.3756 \times 10^{-4}$		$9.5083 \times 10^{-3}$		$5.4164 \times 10^{-4}$		$3.8528 \times 10^{-2}$		$3.1231 \times 10^{-3}$		$1.1283 \times 10^{-1}$	
8	$8.8209 \times 10^{-6}$	3.96	$1.4217 \times 10^{-3}$	2.74	$3.2968 \times 10^{-5}$	4.04	$5.7425 \times 10^{-3}$	2.75	$2.0632 \times 10^{-4}$	3.92	$1.6252 \times 10^{-2}$	2.80
16	$5.5243 \times 10^{-7}$	4.00	$1.9775 \times 10^{-4}$	2.85	$2.0332 \times 10^{-6}$	4.02	$7.9756 \times 10^{-4}$	2.85	$1.3156 \times 10^{-5}$	3.97	$2.1819 \times 10^{-3}$	2.90
32	$3.4765 \times 10^{-8}$	3.99	$2.6298 \times 10^{-5}$	2.91	$1.2761 \times 10^{-7}$	3.99	$1.0597 \times 10^{-4}$	2.91	$8.2908 \times 10^{-7}$	3.99	$2.8336 \times 10^{-4}$	2.95
64	$2.1961 \times 10^{-9}$	3.98	$3.4021 \times 10^{-6}$	2.95	$8.0587 \times 10^{-9}$	3.99	$1.3704 \times 10^{-5}$	2.91	$5.2028 \times 10^{-8}$	3.99	$3.6162 \times 10^{-5}$	2.97



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